

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions, and listings, of claims in the application.

1. (Currently Amended) A method of producing low-temperature coke, in which granular coal is heated to a temperature of 700 to 1050°C in a fluidized-bed reactor ~~[[2]]~~ by ~~means of~~ an oxygen-containing gas, ~~characterized in that~~ comprising introducing from below a first gas or gas mixture ~~is introduced from below~~ through at least one gas supply tube ~~[[3]]~~ into a mixing chamber ~~region (8)~~ of the fluidized-bed reactor ~~[[2]]~~, the at least one gas supply tube ~~[[3]]~~ being at least partly surrounded by a stationary annular fluidized bed ~~[[6]]~~ which is fluidized by supplying fluidizing gas, and ~~that the~~ adjusting gas velocities of the first gas or gas mixture and of the fluidizing gas for the stationary annular fluidized bed ~~(6)~~ are adjusted such that the wherein the gas velocities have a Particle-Froude-Number~~[[s]]~~ in the at least one gas supply tube ~~[[3]]~~ are between 1 and 100, in the stationary annular fluidized bed ~~[[6]]~~ between 0.02 and 2, and in the mixing chamber ~~[[8]]~~ between 0.3 and 30.

2. (Currently Amended) The method as claimed in claim 1, ~~characterized in that~~ wherein the Particle-Froude-Number in the at least one gas supply tube ~~[[3]]~~ is between 1.15 and 20.

3. (Currently Amended) The method as claimed in claim 1 ~~or 2~~, ~~characterized in that~~ wherein the Particle-Froude-Number in the stationary annular fluidized bed ~~[[6]]~~ is between 0.115 and 1.15.

4. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein the Particle-Froude-Number in the mixing chamber ~~[[8]]~~ is between 0.37 and 3.7.

5. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein solids are discharged from the fluidized-bed reactor and separated in a separator, wherein part of the solids or an amount of a product stream discharged from the reactor (2) and separated in a separator (10) are recirculated to the stationary annular fluidized bed ~~[(6)]~~.

6. (Currently Amended) The method as claimed in claim 5, ~~characterized in that~~ wherein the amount of the product stream recirculated to the stationary annular fluidized bed ~~[(6)]~~ is controlled by a ~~in dependence on the pressure difference in pressure~~ above the mixing chamber ~~[(8)]~~.

7. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein the granular coal ~~[(with)]~~ having a grain size of less than 10 mm is supplied to the fluidized-bed reactor (2) as a starting material.

8. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein the granular coal is a highly volatile coal and the highly volatile coal is supplied to the fluidized-bed reactor ~~[(2)]~~ as starting material.

9. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein the fluidizing gas ~~air~~ is supplied to the fluidized-bed reactor ~~is air (2) as fluidizing gas~~.

10. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that the~~ claim 1, wherein pressure in the fluidized-bed reactor ~~[(2)]~~ is between 0.8 and 10 bar.

11. (Currently Amended) The method as claimed in ~~any of the preceding claims, characterized in that~~ claim 1, wherein iron ore is additionally supplied to the fluidized-bed reactor [(2)].

12. (Currently Amended) The method as claimed in claim 11, ~~characterized in that~~ wherein the iron ore is preheated before being supplied to the fluidized-bed reactor [(2)].

13. (Currently Amended) The method as claimed in ~~any of claims 10 to 12, characterized in that~~ claim 10, wherein ~~from the reactor (2) a product of iron ore and low-temperature coke is withdrawn~~ from the fluidized-bed reactor, which wherein the product has a weight ratio of iron to carbon of 1:1 to 2:1.

14. (Currently Amended) A plant for producing low-temperature coke, ~~in particular for performing a~~ by the method as claimed in any of claims 1 to 13, claim 1, comprising a fluidized-bed reactor (2) which constitutes a fluidized-bed reactor, ~~characterized in that~~ wherein the fluidized-bed reactor [(2)] has a gas supply system which is formed such that gas flowing through the gas supply system entrains solids from a stationary annular fluidized bed [(6)], which at least partly surrounds the gas supply system, into the mixing chamber [(8)].

15. (Currently Amended) The plant as claimed in claim 14, ~~characterized in that~~ wherein the gas supply system has at least one gas supply tube [(3)] which in the lower region of the fluidized-bed reactor [(2)] extends upwards substantially vertically into the mixing chamber [(8)] of the fluidized-bed reactor [(2)], the at least one gas supply tube [(3)] being surrounded by a chamber which at least partly annularly extends around the at least one gas supply tube (3) and in which the stationary annular fluidized bed (6) is formed.

16. (Currently Amended) The plant as claimed in claim 15, ~~characterized in that~~ wherein the at least one gas supply tube [(3)] is arranged

approximately centrally ~~based on~~ with reference to the cross-sectional area of the fluidized-bed reactor [(2)].

17. (Currently Amended) The plant as claimed in ~~any of claims 14 to 16, characterized in that~~ claim 14, wherein downstream of the fluidized-bed reactor (2) there is provided a separator [(10)] for separating solids, which ~~preferably~~ has a solids return conduit [(11a)] leading to the annular fluidized bed [(6)] of the fluidized-bed reactor [(2)].

18. (Currently Amended) The plant as claimed in ~~any of claims 14 to 17, characterized in that~~ claim 14, wherein in the annular chamber [(4)] of the fluidized-bed reactor, [(2)] a gas distributor [(5)] is provided, which divides the annular chamber [(4)] into an upper fluidized bed region [(6)] and a lower gas distributor chamber, and that the gas distributor chamber is connected with a supply conduit [(7)] for fluidizing gas.

19. (Currently Amended) The plant as claimed in ~~any of claims 14 to 18, characterized in that~~ claim 14, wherein upstream of the fluidized-bed reactor, [(2)] a preheating stage is provided, which consists of a heat exchanger [(20)] and a separator [(14)].